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# In situ FT-IR studies on the $CO_2$ hydrogenation over the $SiO_2$ -supported RhM (M = Cr, Mo, W) complex catalysts

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## Abstract

The in situ FT-IR spectra were used to study the  $CO_2$  hydrogenation reactions over the SiO<sub>2</sub>-supported heterobinuclear metal complex catalysts, RhM (M = Cr, Mo, W). The bands, which correspond to the formate species adsorbed on the catalysts, were observed. During the hydrogenation reactions, the adsorbed linear and bridged bridging CO were not observed. The experimental results suggest that for the CO<sub>2</sub> and CO hydrogenation reactions over the same catalysts, their catalytic active intermediate species and the reaction mechanisms should be different. © 2001 Elsevier Science B.V. All rights reserved.

Keywords: CO2 hydrogenation; In situ FT-IR; Bimetal complex catalyst

# 1. Introduction

The hydrogenation of CO<sub>2</sub> to valuable chemicals has received much interest in the recent years. The Cu–ZnO based catalysts are well known to be active for the methanol synthesis through the hydrogenation of CO or CO<sub>2</sub>. The Cu-formate species on surface are regarded as the intermediates of the conversion from CO<sub>2</sub> to methanol [1,2]. However, the reaction mechanisms of the active species on the Cu based catalysts are still not clear. Until now, the supported noble bimetal catalysts for the CO<sub>2</sub> hydrogenation to methanol have not been intensively studied yet. We reported the experimental results about the SiO<sub>2</sub>-supported heterobinuclear metal complex catalysts, (dppe) Rh( $\mu$ -CO) M(CO)<sub>3</sub> (M = Cr, Mo, W; dppe = Ph<sub>2</sub>P(CH<sub>2</sub>)<sub>2</sub>PPh<sub>2</sub>) [3], (I). The complex

\* Corresponding author. *E-mail address:* shaocp@ms.dicp.ac.cn (C. Shao). catalysts exhibit high activity and selectivity for the methanol synthesis from  $CO + H_2$  [4] and  $CO_2 + H_2$  [5,6].

The present paper reports the in situ FT-IR results of the species adsorbed on the RhM/SiO<sub>2</sub> catalysts during the CO<sub>2</sub> hydrogenation reactions.

#### 2. Experimental

## 2.1. The preparation of the catalysts

The catalysts were prepared using the impregnation method. The complexes (I) were used as the catalyst precursors. Prior to impregnation, silica was evacuated at 673 K for 2 h to remove physically absorbed water, and then an appropriate amount of THF solution of (I) was poured into the silica. After the impregnation process was completed, the catalysts were dried under vacuum at room temperature.

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## 2.2. The measurement of in situ IR spectra

The in situ IR spectra were measured using an IR stainless steel reactor cell with a CaF<sub>2</sub> window. The catalysts, pressed into a 10 mm diameter disk, were placed in the cell, which was used as a reactor. The spectra were recorded using a Perkin-Elmer FT-IR 2000 spectrometer with a resolution of  $2 \text{ cm}^{-1}$ . The pressure of the CO<sub>2</sub> and H<sub>2</sub> atmosphere was kept at 0.1 MPa with a constant flow-rate ration (H<sub>2</sub>/CO<sub>2</sub> = 3:1). The reaction temperature was increased to a certain temperature under vacuum and was kept for 15 min. The CO<sub>2</sub> and H<sub>2</sub> gases were passed through the reactor cell at this reaction temperature for 15 min, and at the same time the in situ FT-IR spectra were recorded under the CO<sub>2</sub> hydrogenation condition.

#### 3. Results and discussion

Figs. 1–3 show the in situ FT-IR spectra of the 3 wt.% RhM/SiO<sub>2</sub> catalysts during the CO<sub>2</sub> hydrogenation reaction temperatures.



Fig. 1. In situ IR spectra of Rh-Cr/SiO<sub>2</sub> catalyst at various temperature in  $CO_2 + H_2$  flow: (a) 413; (b) 473; (c) 533 K.



Fig. 2. In situ IR spectra of Rh-Mo/SiO<sub>2</sub> catalyst at various temperature in  $CO_2 + H_2$  flow: (a) 413; (b) 493; (c) 533 K.

As shown in Fig. 1, on RhCr/SiO<sub>2</sub>, the bands at 2000,  $1992 \text{ cm}^{-1}$  (terminal CO) and  $1763 \text{ cm}^{-1}$ (bridging CO), which are attributed to co-ordinated CO of the original complex, decrease evidently and even disappear (for terminal CO) when the reaction temperature is increased from 413 to 513 K. The bands at 1482 and  $1434 \text{ cm}^{-1}$  still remain and the bands are attributed to co-ordinated PPh3 of the original complex. The bands at 2360 and  $2337 \text{ cm}^{-1}$ , which are attributed to CO<sub>2</sub> in gas phase, are too strong to be canceled. At the same time, a new strong sharp band appears at 1586 cm<sup>-1</sup> and its intensity increases evidently with increasing the reaction temperature from 413 to 533 K. At  $1313 \text{ cm}^{-1}$  appear some weak bands, which can be assigned to the stretching frequency of the formate species adsorbed on Rh of RhCr. Similar bands were previously reported, which were ascribed to the formate species adsorbed on Cu or Rh during the  $CO_2$  hydrogenation reaction; e.g. the bands at 2933, 2858, 1591 and  $1353\,\mathrm{cm}^{-1}$  for Cu/SiO<sub>2</sub> [7]; at 1548 cm<sup>-1</sup> for Cu/SiO<sub>2</sub> [8]; at 2956, 2883, 1560,  $1351 \text{ cm}^{-1}$  for Cu/TiO<sub>2</sub> [7]; at  $1585 \text{ cm}^{-1}$  for



Fig. 3. In situ IR spectra or Rh-W/SiO<sub>2</sub> catalyst at various temperature in  $CO_2 + H_2$  flow: (a) 413; (b) 493; (c) 533 K.

Cu(Zn)/SiO<sub>2</sub>; at 1595, 1380 cm<sup>-1</sup> for Cu/ZnO/Al<sub>2</sub>O<sub>3</sub> [9]; at 1568,  $1373 \text{ cm}^{-1}$  for CuO/TiO<sub>2</sub> [10]; and at 1511, 1378 cm<sup>-1</sup> for Rh-Li/SiO<sub>2</sub> [11], etc. Recently, Bettahar et al. reported that there are three types of formate species adsorbed Zn/Al2/O3: the bands at 2881, 2744, 1595, 1375 cm<sup>-1</sup>; at 1650, 1320 cm<sup>-1</sup>; at 2895, 2767, 1590, 1390, 1370 cm<sup>-1</sup>; and a formate specie adsorbed on Cu at 2825, 2847, 2692,  $1352 \,\mathrm{cm}^{-1}$  during the CO<sub>2</sub> hydrogenation reaction over the Cu-Zn Al<sub>2</sub>O<sub>4</sub> catalyst [12]. Therefore, these formate species adsorbed on Rh or RhM can be regarded as an intermediate of the methanol synthesis from the CO<sub>2</sub> hydrogenation reaction. The intensity of the band at 1586 cm<sup>-1</sup> increases with increasing the reaction temperature. It is reasonable taking into account that the catalytic activity increases with increasing the reaction temperature [5,6].

Similarly, as shown in Figs. 2 and 3, on RhMo/SiO<sub>2</sub> and RhW/SiO<sub>2</sub>, the bands, which are attributed to co-ordinated CO of the original complexes, also decrease when the reaction temperature is increased from

413 to 533 K. The band, attributed to co-ordinated bridging CO, shifts to a lower wave number (from 1763 to 1753 cm<sup>-1</sup>). At the same time, the intensities of the bands ascribed to the formate species adsorbed on Rh of RhM also increase when the reaction temperature is increased, and the same weak band at  $1313 \text{ cm}^{-1}$  also appears. The bands at 1481,  $1434 \text{ cm}^{-1}$ , which are attributed to co-ordinated PPh<sub>3</sub> of the original complexes, still remained. It indicates that the RhM/SiO<sub>2</sub> catalysts are still stable at 533 K.

The FT-IR spectra of the CO<sub>2</sub> hydrogenation reactions on the RhM (M = Cr, Mo and W)/SiO<sub>2</sub> catalysts at the same reaction temperature are shown in Fig. 4 (493 K) and Fig. 5 (533 K). As shown in Fig. 4, all the bands, which are attributed to co-ordinated terminal CO at 1991, 1968 cm<sup>-1</sup> and bridging CO at 1763 cm<sup>-1</sup>, still remained with proper intensities. The bands at 1584 cm<sup>-1</sup>, attributed to the formate species adsorbed on Rh of RhM, become stronger. The intensity of the band for RhMo/SiO<sub>2</sub> is stronger than that for RhCr/SiO<sub>2</sub> or RhW/SiO<sub>2</sub>. All the bands at 1481 and 1435 cm<sup>-1</sup>, attributed to co-ordinated



Fig. 4. In situ IR spectra of three catalysts at 493 K in  $\text{CO}_2 + \text{H}_2$  flow: (a) Rh-Cr/SiO<sub>2</sub>; (b) Rh-Mo/SiO<sub>2</sub>; (c) Rh-W/SiO<sub>2</sub>.



Fig. 5. In situ IR spectra of three catalysts at 533 K in  $\text{CO}_2 + \text{H}_2$  flow: (a) Rh-Cr/SiO<sub>2</sub>; (b) Rh-Mo/SiO<sub>2</sub>; (c) Rh-W/SiO<sub>2</sub>.

PPh<sub>3</sub>, still remained with proper intensities. Fig. 5 shows that the intensities of the bands, attributed to co-ordinated CO, obviously decrease and even disappear (for RhCr/SiO<sub>2</sub>). However, the bands, attributed to co-ordinated bridging CO, shift to  $1755 \text{ cm}^{-1}$ . The bands attributed to the formate species adsorbed on Rh of RhM become stronger than those at 493 K. The result indicates that the formate species adsorbed or Rh of RhM are catalytically active for the CO<sub>2</sub> hydrogenation reaction, which produces methanol. The hydrogenation process of the formate species is probably the rate-determining step. The in situ FT-IR spectra of the SiO<sub>2</sub>-supported complex catalysts exhibit notable difference from those of the SiO<sub>2</sub>-supported Rh catalyst during the CO<sub>2</sub> hydrogenation reaction. The latter show the strong bands at 2040 and  $1806 \,\mathrm{cm}^{-1}$ , which are assigned to the linear and bridged CO species adsorbed on Rh [11].

These results are obviously different from the result of the CO hydrogenation over the same catalysts previously reported. For the spectra of the CO hydrogenation, co-ordinated bridging CO disappear firstly, and then co-ordinated terminal CO disappear. Some new bands appear at 2058 1997 and 2004 cm<sup>-1</sup> for Rh-Cr/SiO<sub>2</sub>, RhMo/SiO<sub>2</sub>, and RhW/SiO<sub>2</sub>, respectively. They are attributed to the linear CO species adsorbed on Rh, but the band attributed to the adsorbed bridged CO species [13] does not appear. However, for the CO<sub>2</sub> hydrogenation reaction, the bands attributed to the adsorbed linear and bridged CO species do not appear. The bands at  $1589 \,\mathrm{cm}^{-1}$ , ascribed to the formyl species adsorbed on Rh for all the RhM/SiO<sub>2</sub> catalysts during the CO hydrogenation reaction, are weak and broad. However, the bands at  $1585 \,\mathrm{cm}^{-1}$ , ascribed to the formate species adsorbed on Rh for RhM/SiO<sub>2</sub> catalysts during the CO<sub>2</sub> hydrogenation reaction, are strong and sharp. The results indicate that the mechanisms of the CO and CO<sub>2</sub> hydrogenation reactions over the same RhM/SiO<sub>2</sub> catalysts should be different. The following mechanism of the CO<sub>2</sub> hydrogenation reaction over the RhM/SiO<sub>2</sub> catalysts is suggested. The CO<sub>2</sub> gas molecules are readily adsorbed by the catalysts, and the adsorbed CO<sub>2</sub> species on the catalytic site are rapidly converted to the formate species adsorbed on Rh or RhM under the reaction conditions. The formate species are hydrogenated to methanol, and the process is probably a rate-determining step. Therefore, the formate species adsorbed on Rh or RhM can be regarded as a major intermediate for the methanol synthesis from the CO<sub>2</sub> hydrogenation. The CO molecules produced in the CO<sub>2</sub> hydrogenation should result from the reverse water gas shift reaction.

## 4. Conclusions

In situ FT-IR was used to study the methanol synthesis reaction from the  $CO_2$  hydrogenation over the RhM/SiO<sub>2</sub> catalysts. Some special formate species with an OCO asymmetric band at 1586 cm<sup>-1</sup> is observed. The formate species are probably bound to Rh or RhM, and are active intermediates.

The comparison between the in situ FT-IR results of  $CO_2/H_2$  and  $CO/H_2$  under the same reaction conditions shows that the produced surface species for the two reaction systems are essentially different. Under  $CO/H_2$  atmosphere, no adsorbed formate species can be observed.

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